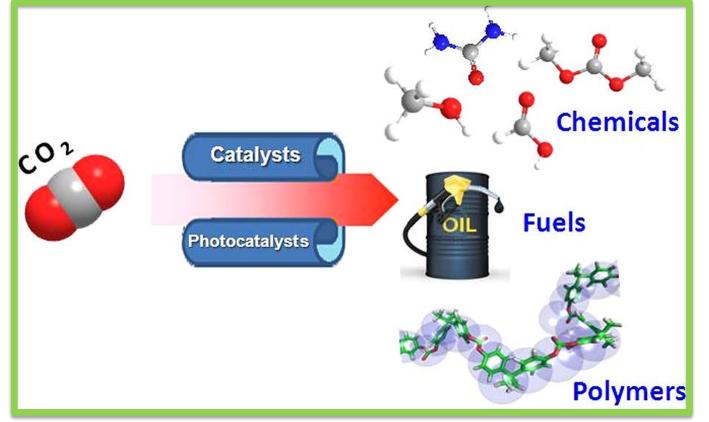
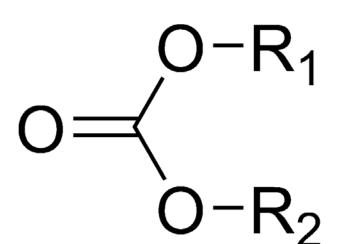
# CO<sub>2</sub> Remediation

- CO<sub>2</sub> is considered a very important greenhouse gas correlated with global Earth temperatures.
- In 2012, U.S. CO<sub>2</sub> emissions were 5.35 *Billion* tons of CO<sub>2</sub> with two thirds from combustion for power generation and transportation.
- With such a reliance on combustion chemistry, the elimination of  $CO_2$  production would be extremely disruptive.
- A better solution is to recycle generated CO<sub>2</sub> for a carbon cycle similar to that found in nature and allowing valorization of this abundant waste chemical.



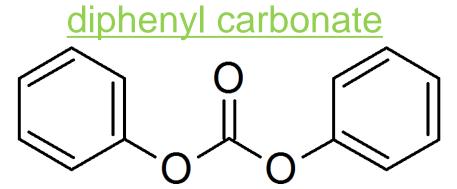
#### **Organic Carbonates**

• Organic carbonates are a class of organic chemicals containing a carbonate ester.

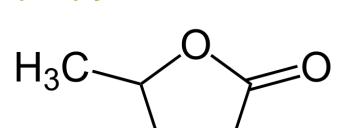


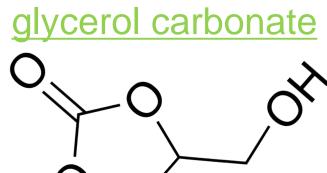
• The simplest organic carbonates contain two R functional groups.

$$\frac{\text{dimethyl carbonate}}{H_3C_0CH_3}$$

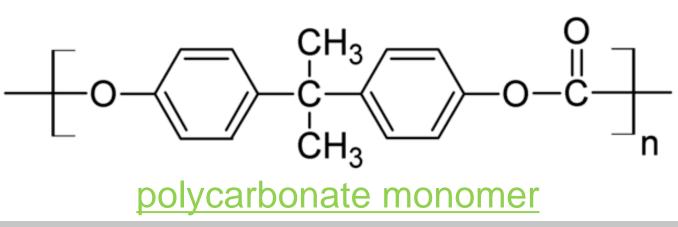


• More complex carbonates can be made by substituting other R groups, or by connecting together R groups to form cyclic carbonates. propylene carbonate alvcerol carbonate





• One application of organic carbonates are for the synthesis of polycarbonate plastics.





References: <sup>1</sup> Aresta, Chem Rev (2014) 114, 1709-1742

# Valorization of CO<sub>2</sub> to Organic Carbonates with Cerium Oxide Chris Marin & Dr. Chin Li Cheung

Contact: ccheung2@unl.edu

# Why Dimethyl Carbonate (DMC)?

# $2 CH_3 OH$

methanol

carbon dioxide

- ceria catalys
- Model system for generating more complex carbonates from  $CO_2$ . Proposed as an oxygenated fuel additive compound.
- DMC is a VOC exempt organic solvent used by the coatings industries.
- Commercially converted to diphenyl carbonate, which is polymerized to produce polycarbonate plastics – <u>permanently capturing CO<sub>2</sub> while</u> generating valuable products.
- For DMC to be used as a fuel additive or for polycarbonate to be a commodity plastic, need a direct way to synthesize organic carbonates.

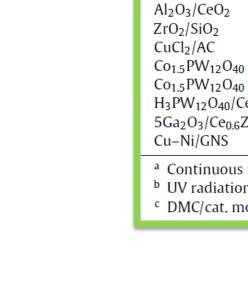
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#### **DMC Background**

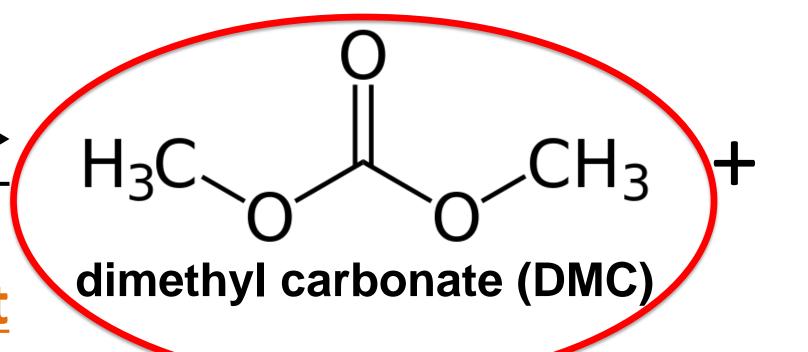
- Until 1980, DMC was produced by the phosgenation of methanol - abandoned due to the high toxicity of phosgene.
- Currently made by the oxy-carbonylation of methanol and the carbonylation of methylnitrile both routes using toxic and corrosive chemicals.
- Current direct synthesis catalysts offer poor DMC yields and slow rates.

Catalyst	Operating conditions	Time	Yield/selec.
ZrO <sub>2</sub>	433 K	2 h	0.3/100%
Ni(CH <sub>3</sub> COO) <sub>2</sub> ·4H <sub>2</sub> O	413 K; 7.0 MPa	12 h	2.1/45%
H <sub>3</sub> PO <sub>4</sub> /ZrO <sub>2</sub>	403 K	2 h	0.3/100%
H <sub>3</sub> PO <sub>4</sub> /ZrO <sub>2</sub>	403 K	2 h	0.3/100%
CeO <sub>2</sub> –ZrO <sub>2</sub>	383 K; 6.0 MPa	4 h	0.8/100%
$H_3PO_4/V_2O_5$	453 K; 0.6 MPa	_a	1.8/93%
Cu-Ni/V2O5-SiO2	413 K; 0.9 MPa	_a	2.4/87%
CeO <sub>2</sub>	403 K	5 h	0.8/100%
Cu (Ni, V, O) <sup>b</sup>	393 K; 1.2 MPa	-	4.5/90%
Cu (Ni, V, O)	393 K; 1.2 MPa	-	3.5/93%
H <sub>3</sub> PW <sub>12</sub> O <sub>40</sub> /Ce <sub>0.1</sub> Ti <sub>0.9</sub> O <sub>2</sub>	443 K	12 h	5/100%
Al <sub>2</sub> O <sub>3</sub> /CeO <sub>2</sub>	408 K; 5.0 MPa	3 h	0.4/100%
$ZrO_2/SiO_2$	423 K; 20 MPa	80 h	6 <sup>c</sup> /100%
CuCl <sub>2</sub> /AC	398 K; 1.2 MPa	4 h <sup>b</sup>	-/90%
Co <sub>1.5</sub> PW <sub>12</sub> O <sub>40</sub>	353 K; 0.25 MPa	5 h	1.1/69%
Co <sub>1.5</sub> PW <sub>12</sub> O <sub>40</sub>	473 K; 0.1 MPa	_b	7.6/86.5%
H <sub>3</sub> PW <sub>12</sub> O <sub>40</sub> /Ce <sub>0.6</sub> Zr <sub>0.4</sub> O <sub>2</sub>	443 K; 6.0 MPa	3 h	1.2/100%
5Ga <sub>2</sub> O <sub>3</sub> /Ce <sub>0.6</sub> Zr <sub>0.4</sub> O <sub>2</sub>	443 K; 6.0 MPa	3 h	2.3/100%
Cu–Ni/GNS	373 K; 1.2 bar	3 h <sup>b</sup>	5/92%
<sup>a</sup> Continuous reactor.			
<sup>b</sup> UV radiation.			
<sup>c</sup> DMC/cat. molar ratio.			

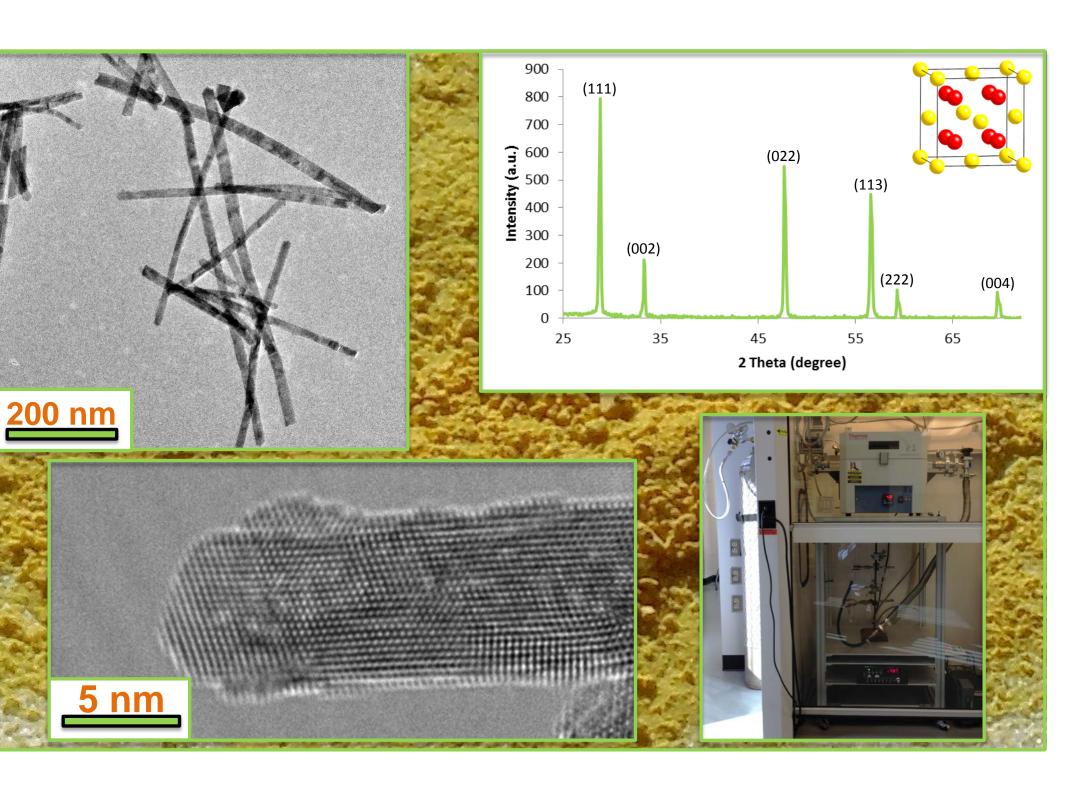
- While the direct synthesis is exothermic (-20.10 kJ/mol), the entropy change is negative and the reaction only favors products at low temps.
- Due to poor kinetics, reactions currently done at high temp, meaning catalyst improvements are essential



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# Ceria Background

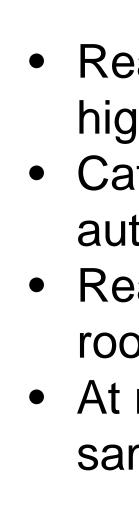


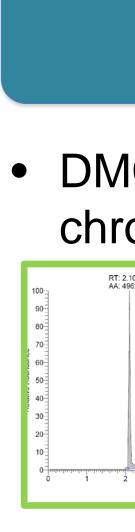
- We synthesize ceria catalyst hydrothermally as cerium hydroxide nanorods.
- Conversion to cerium oxide (ceria) occurs by programmed calcination in air or  $O_2$ .
- Ceria surface is incompletely coordinated and takes a mixture of +3 and +4 oxidation states. Fluctuating valency of ceria allows oxide mobility and amphoteric catalytic behavior • By controlling the system pressure for the calcination step, can control the ratio of +3 ceria to +4 ceria.
- Large aspect ratio ceria rods maximize surface area even at elevated temperatures.



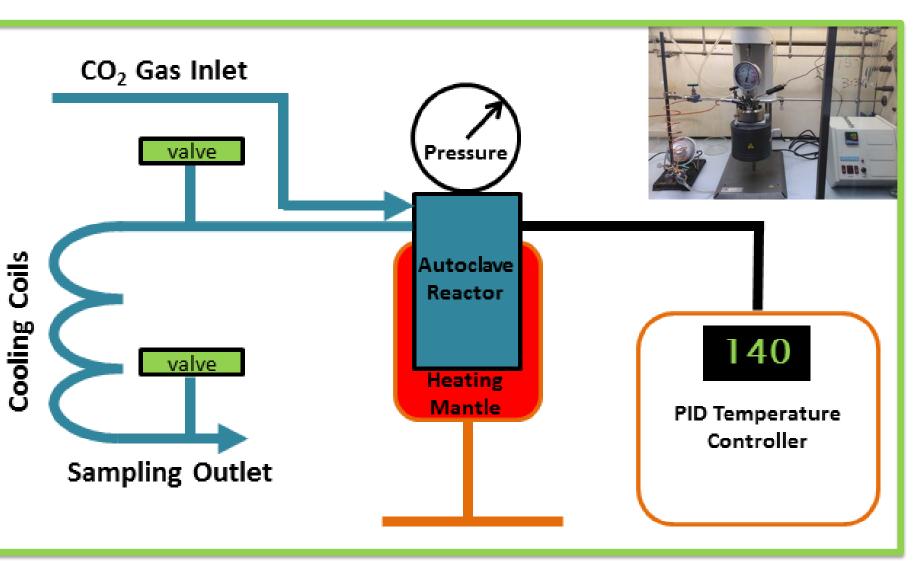
water







#### **High Pressure Chemistry**



Reactions performed in a stirred and heated high pressure autoclave with a 3000 psi limit. Catalyst and anhydrous methanol are sealed in autoclave reactor.

• Reactor pressurized with CO<sub>2</sub> to 800 psi at room temperature.

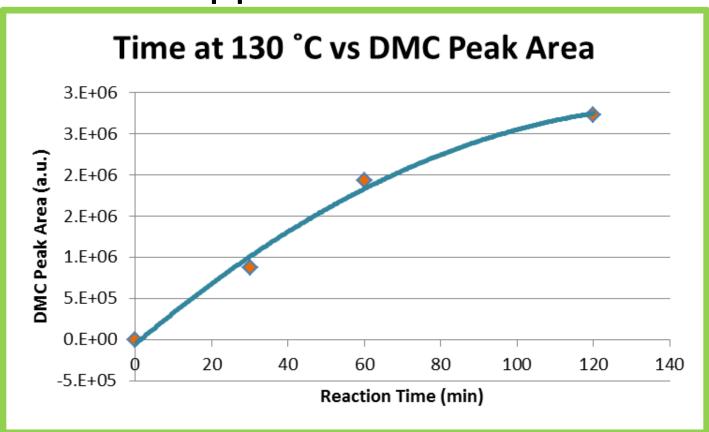
• At reaction temperature and pressure, product sampled at regular intervals with sampling line.

### Analysis + Results

• DMC concentration is monitored by gas chromatography – mass spectrometry (GCMS).

<sup>2.10</sup> 4962575 <b>30 min</b>	<sup>100</sup> 90	100 100 90
	80 70 60 40 50 9	
DMC RT: 2.39 AA: 45580 RT: 3.26 AA: 873099 2 3 4 5 6 7 Time (min)	20 10 0 1 0 1 1 2 0 1 1 2 1 1 2 1 1 2 1 1 2 1 1 2 1 1 2 1 1 2 1 1 1 2 1 1 2 1 1 2 1 1 2 1 1 2 1 1 2 1 1 1 1 1 1 1 1 1 1 1 1 1	20 10 0 11 0 0 1 1 20 10 0 1 20 10 0 1 1 2 1 2 1 2 1 2 1 1 2 1 1 2 1 1 2 1 1 2 1 1 2 1 1 2 1 1 2 1 1 2 1 1 2 1 1 2 2 1 2 1 2 1 2 1 2 2 2 2 2 2 2 2 2 2 2 2 2

 Initial rate of DMC generation is linear with respect to time, but rate slows down as equilibrium is approached.



• By keeping the initial concentrations of CO<sub>2</sub> and methanol constant, the initial DMC formation rate gives the rate constant.

• The activation energy for the reaction over a specific catalyst is found by measuring the rate constant at multiple temperatures and fitting an Arrhenius curve.